



Recent advances in layered double hydroxides (LDHs) as two-dimensional membrane materials for gas and liquid separations



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ABSTRACT

Membrane-based technology represents an emerging strategy for energy-efficient gas/liquid separation. Among various factors, dimensionality and microstructure of membrane materials played a dominant role in determining their separation performance. Recently, unique structural properties of two-dimensional (2D) nanomaterials with atomic size thickness are rapidly emerging as desirable building blocks for the design of high performance membranes. Among them, layered double hydroxides (LDHs), a representative of anionic clays, have attracted extensive interest and exhibited promising prospects for membrane applications due to their uniform interlayer galleries, which may permit precise molecular sieving in case the gallery height was comparable with kinetic diameters of guest molecules. Moreover, highly tunable chemical compositions and gallery height as well as the rich surface functionality of LDH building blocks further endowed them with unprecedented opportunities for efficient gas/liquid separation. This paper summarizes recent breakthrough in LDH-based separation membranes with particular emphasis on the opportunities and challenges facing their commercial applications.

1. Introduction of two-dimensional membrane materials

Recently, unique physicochemical properties of two-dimensional (2D) nanomaterials with atomic layer thickness are rapidly emerging as superb building blocks for designing molecular sieve membranes surpassing the Robeson upper-bound [1–4]. The integration of 2D nanomaterials enables the formation of an ultrathin separation layer which promises unprecedented permeability and selective diffusion paths (interlayer galleries & in-plane pores) [5]. In addition, further incorporating 2D nanosheets into the polymer matrix, resulting in the formation of mixed matrix membranes (MMMs), is considered as a promising strategy for simultaneous improvement of both permeability and selectivity of polymer membranes [6,7]; moreover, their mechanical strength is anticipated to be improved either. At present, studies on 2D layered membranes are mainly focused on zeolites (e.g., exfoliated MFI nanosheets) [3,8–11], graphene-based materials [12–15], transition metal dichalcogenides (TMDCs) [16], metal-organic frameworks (MOFs) [17–19], covalent organic frameworks (COFs) [20–23], ionic clays (e.g. Montmorillonite [24,25] and anionic layered double hydroxides (LDHs) [26]). LDHs, also commonly called hydrotalcite-like compounds, are representative of anionic layered materials composed

of positively charged brucite-like 2D sheets, charge compensating anions and solvation molecules located in interlayer galleries [27,28]. Compositional flexibility and gallery height adjustability of LDHs give rise to a functional diversity. Furthermore, microstructures of LDHs can be easily tuned by changing the synthetic strategy [29]. At present, LDHs have shown widespread applications in CO₂ adsorption [30–33], catalysts [34–37], polymeric modification [28,38,39], electrochemistry [40] and controlled drug delivery [41].

1.1. Chemical composition and structure of LDHs

Hydrotalcite, which was first discovered in Sweden and subsequently gave its name to a large mineral group of naturally occurring LDHs [42], could be expressed by the formula [Mg₆Al₂(OH)₁₆]CO₃·4H₂O [43]. Framework structures of naturally occurring LDHs, which could be expressed in rhombohedral and hexagonal forms, respectively, were indicated in Fig. 1(a) and (b). LDHs are made of layers of metal cations (M²⁺ and M³⁺) with similar ionic radii. These metal cations occupy the centers of edge sharing octahedra, whose vertexes contain hydroxide ions that connect to form infinite 2D sheets [27]. A general molecular formula of LDHs can be expressed as

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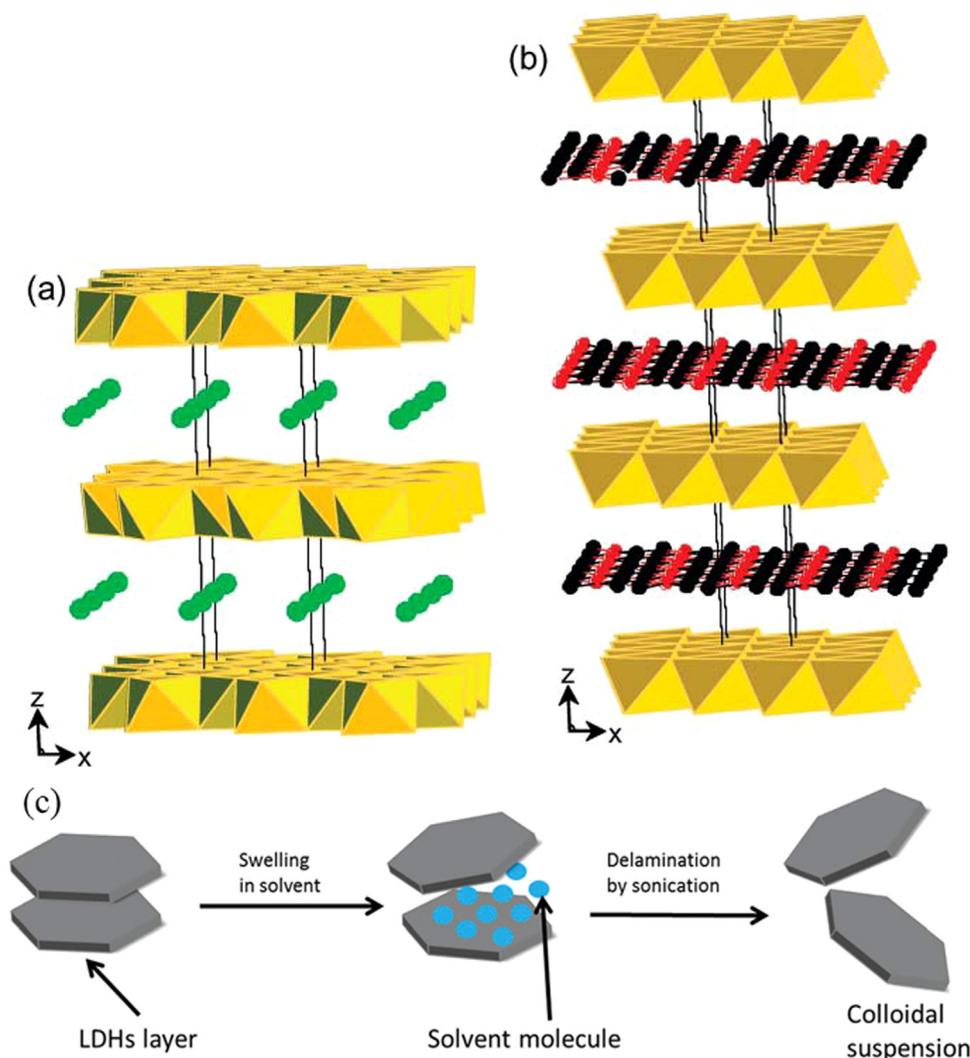


Fig. 1. Schematic structure of LDHs showing the polymorphic stacking patterns: (a) hexagonal, (b) rhombohedral. Reproduced with permission from Ref. [42]. Copyright © 2002, Royal Society of Chemistry. And (c) a generalized procedure for exfoliation of bulk LDHs. Reproduced with permission from Ref. [50]. Copyright © 2017, Royal Society of Chemistry.

$[M_{1-x}^{2+}M_x^{3+}(\text{OH})_2][A^{n-}]_{x/n}m\text{H}_2\text{O}$, where M^{2+} represents divalent metal ions (such as Mg^{2+} , Zn^{2+} , Cu^{2+} or Ni^{2+}), M^{3+} represents trivalent metal ions (such as Al^{3+} , Fe^{3+} , Ga^{3+} , or Mn^{3+}) and A^{n-} represents charge compensating anions (such as CO_3^{2-} , NO_3^- , SO_4^{2-} , and stearate). Normally the x value is confined between 0.2 and 0.4 [26,28,30,31,39,44–47]. Compared with other layered materials, LDHs displays unique structural and physicochemical properties such as (1) multiple alternative metal cations allowing chemical compositions of host layers to be controlled precisely; (2) substitutable interlayer anions contributing to adjustable gallery height and surface functionality; (3) the unique memory effect endowing LDHs with the restorability to their original layered structures [48,49]. To summarize, the rich intercalation chemistry, surface functionality and unique memory effect of LDHs make them superb candidates for high performance membranes.

1.2. Preparation of delaminated LDHs and post-treatment of LDHs

In the past few years, diverse methods, including co-precipitation, hydrothermal synthesis, ion-exchange and calcination-reconstruction [50], have been developed for the preparation of LDHs with controllable microstructures. Among them, the co-precipitation method generally produces uniform LDHs with a wide grain-size range (10 nm to 1 μm) and lower crystallinity, which was more favorable for selective

anion-exchange intercalation and exfoliation [51]. In contrast, the urea hydrolysis method normally led to the formation of carbonate-intercalated LDHs with larger size (microns in diameter), higher crystallinity and purity [52].

Conventionally synthesized LDHs are composed of uniformly stacked brucite-like nanosheets with a thickness of 0.48 nm [53]. Exfoliation of bulk LDHs into single-layer nanosheets enabled to maximize the surface area and re-adjust the gallery height during drying-reconstruction process [54,55], which was favorable for their utilization as high performance separation membranes [56–58]. Normally LDHs could be exfoliated by using formamide as the solvent [54] or organic anions as charge-compensating anions (e.g. anionic surfactants [59]) under ultrasonication (as shown in Fig. 1(c)) [50]. Particularly, it was noted that Wang [55] reported that the delamination degree of LDHs in formamide could be determined by simply analyzing formed LDH dispersion gels with XRD (Fig. 2), which was quite facile and convenient.

Furthermore, in order to maximize their separation performances, it is critical to prepare LDH-polymer MMMs in which LDH sheets/particles were well-dispersed. However, owing to the intrinsic hydrophilic nature of LDHs, they generally could not be well dispersed in nonpolar solvents. Therefore, post-treatment of LDHs with solvent has become a simple and cost-effective method for preparation of stable and transparent dispersion of the hydrophilic LDHs (Fig. 3(a) and (b)) [46]. For

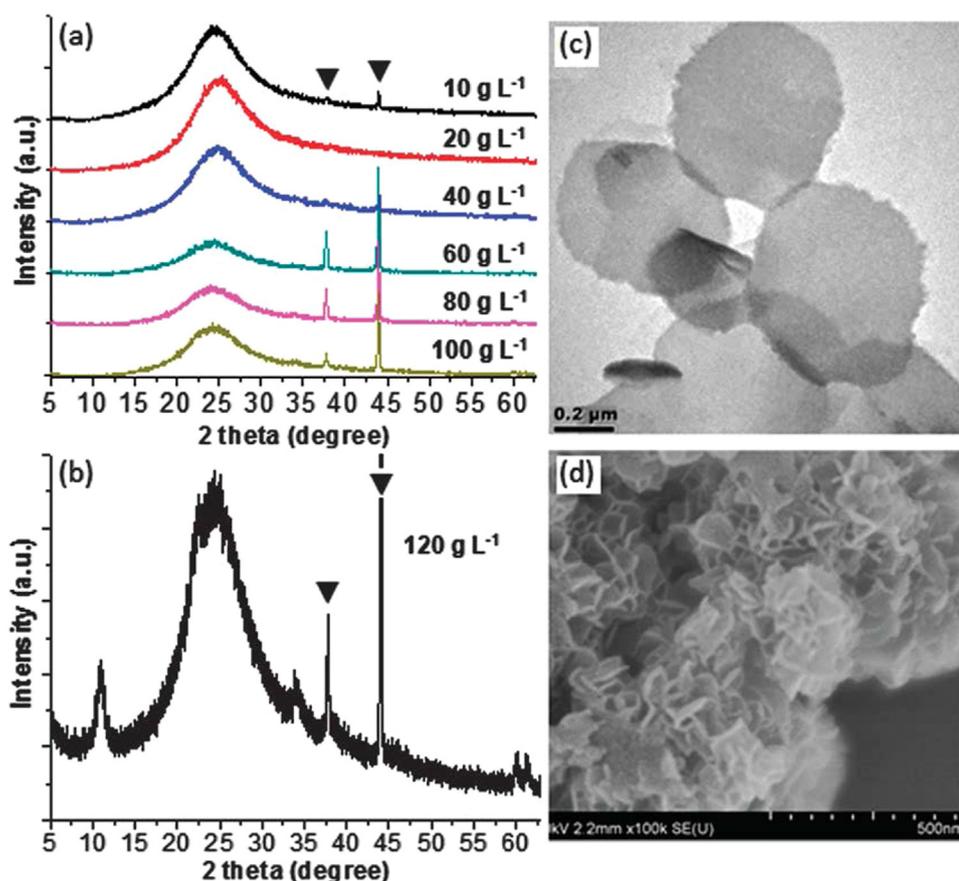


Fig. 2. (a, b) XRD patterns of delaminated Mg–Al–NO₃ LDH dispersion gels with concentrations from 10 to 120 g L⁻¹; (c) the HR-TEM image and (d) SEM image of MgAl–NO₃ LDHs. (▼) sample holder. Reproduced with permission from Ref. [55]. Copyright © 2014, Royal Society of Chemistry.

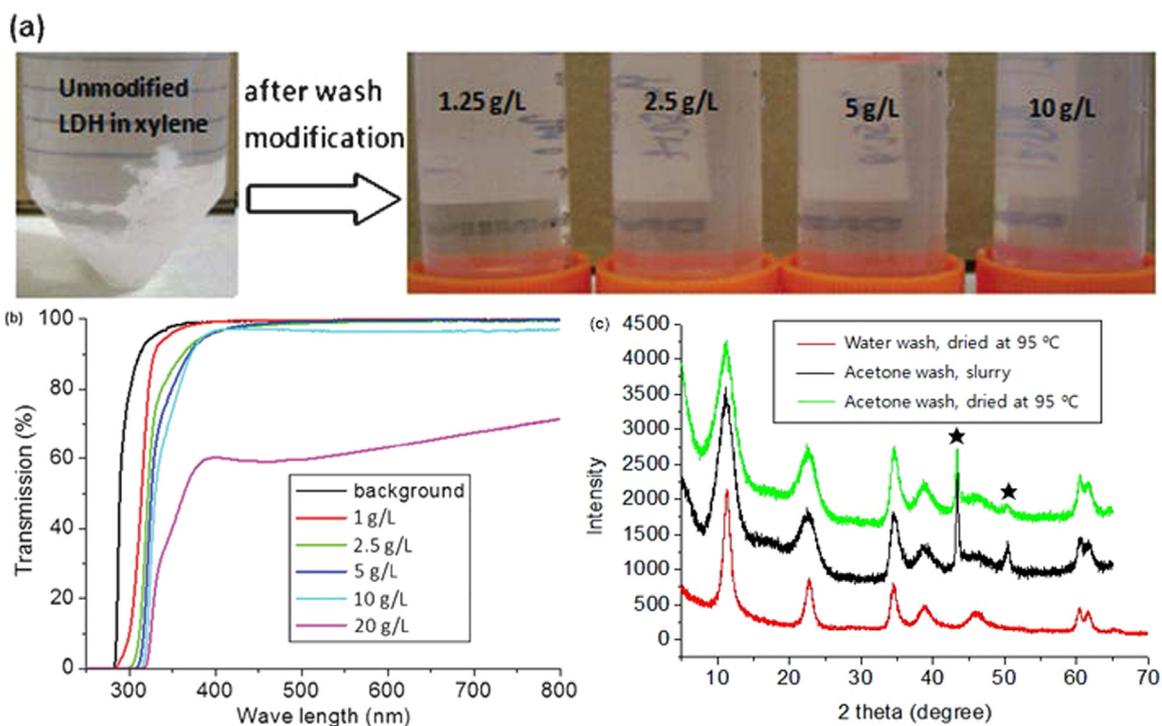


Fig. 3. Illustration of the effect of solvent post-treatment on hydrophobicity of MgAl-LDH nanoparticles. (a) Normally unmodified LDHs could not be dispersed in xylene; in contrast, LDHs nanoparticles could be well dispersed in xylene by washing modification; (b) UV–visible spectra of solvent-modified MgAl-LDHs in xylene; (c) XRD patterns of MgAl–CO₃ LDHs after washing with water or acetone, (★) sample holder. Reproduced with permission from Ref. [46]. Copyright © 2012, Royal Society of Chemistry.

instance, obtained LDH slurry was sequentially washed with equimolar water/ethanol three times and acetone three times which did not change their composition, structure or particles size (see Fig. 3(c)). Afterwards, solvent-modified LDH nanoparticles could be well dispersed in xylene giving rise to formation of a stable suspension. It seems very promising that this procedure could be further extended to diverse LDH-polymer MMMs.

Potential applications of LDHs as high-performance separation membranes, which has become a hot research topic in recent years [57,60–62], have not been systematically summarized yet. This review summarized recent progress made in LDH-based separation membranes with particular focus on their unique adsorption, diffusion and molecular sieving behaviors essential for high-efficiency membrane separation. To the best of our knowledge, this represented the first review article focusing on potential applications of LDH-based separation membranes. In the following sections, we emphasize on the application of LDH-based membranes in gas and liquid separations, respectively.

2. LDH-based membranes for gas separation

2.1. LDHs as separation layers

LDHs as a representative of anionic 2D materials, not only exhibited high-affinity interaction with specific guest molecules [63], but also enabled to accurately tune the gallery height from nanometer to sub-nanometer scale. Recent progress made in the development of asymmetric LDH membranes has confirmed its great potential for efficient gas separation. Tsotsis [64] first employed a vacuum-suction approach for the preparation of MgAl-CO₃ LDH asymmetric membranes. Prepared LDH membranes showed an ideal CO₂/N₂ separation factor (SF) as high as 35 after repair of cracks and defects within LDH membranes by silicone coating. In the next step, electrophoretic deposition (EPD) technique was further employed to deposit LDH membranes on macroporous α -Al₂O₃ substrates. Prepared LDH membranes showed preferred selectivity towards CO₂, which was consistent with previous studies demonstrating their great potential as superb CO₂ adsorbents [65]. Caro's group was committed to extending the utilization of LDH membranes in H₂ purification. Well-intergrown NiAl-CO₃ LDH membranes were successfully prepared on mesoporous γ -Al₂O₃ substrates by in situ hydrothermal growth [66]. XRD pattern indicated a uniform gallery height of 0.31 nm, which was smaller than kinetic diameters of most gas molecules except H₂ (0.29 nm) (Fig. 4). Correspondingly, the SF of activated LDH membranes reached ~80 for H₂/CH₄, making them particularly attractive for H₂ purification (Fig. 4c). Furthermore, it was further found that the concentration of CO₂ dissolved in the precursor solution played an important role in controlling the preferred orientation of LDH membranes [67]. Trace amount of CO₂ induced formation of *ab*-oriented 0.6 μ m-thick LDH membranes (Fig. 4(d)), whereas oversaturated CO₂ resulted in formation of randomly oriented 5 μ m-thick LDH membranes (Fig. 4(e)). Experimental results demonstrated that both *ab*- & randomly oriented LDH membranes showed clear size-based selectivity. However, randomly oriented LDH membranes showed much higher H₂ selectivity possibly due to decreased mesoscopic defects. It should be emphasized that compared with the manufacturing process of graphene oxide (GO) or other 2D membranes, nucleation of LDH crystallites, their attachment to substrates and final formation of defect-free LDH membranes could be completed in one step [67].

2.2. LDHs as precursor layers

LDH membranes also enabled to significantly enhance the separation performance of MOF membranes. Caro successfully prepared ZIF-8-ZnAl-NO₃ LDH composite membrane in one step by partial conversion of 2.5 μ m-thick ZnAl-NO₃ LDH precursor membranes (Fig. 5) [68]. Partial dissolution of ZnAl-NO₃ LDH precursor membranes led to reduced framework density and thickness (~1.3 μ m), leading to

significantly enhanced H₂ permeance. Moreover, since there existed two gas selective layers, prepared ZIF-8@ZnAl-NO₃ LDH composite membranes showed significantly enhanced gas selectivity (H₂/CH₄ and CO₂/CH₄ SF reached 54.1 and 12.9, respectively), which was significantly higher than former ZIF-8 and ZnAl-NO₃ LDH separation membranes [5].

2.3. LDHs as complementary buffer layers

LDHs could also serve as modifier for preparation of high performance ZIF membranes. Liu [69] prepared preferentially vertically aligned MgAl-CO₃ LDH layers on α -Al₂O₃ substrates by facile in situ hydrothermal growth. ~1.7 μ m-sized LDH crystals showed typical plate-like morphology with mutual distances of ~1 μ m. LDH layer-modified substrates were then covered with uniform zeolitic imidazolate frameworks (ZIF-8) seed layers by dip-coating. Owing to the hindrance from adjacent LDH walls, trapped ZIF-8 seeds were firmly attached to substrates. After secondary growth, well-intergrown ZIF-8 membranes were formed. The single gas permeability results demonstrated the SF of H₂/CO₂, H₂/N₂, and H₂/CH₄ gas pairs reached 4.2, 9.4, and 12.9, respectively, and related H₂ permeance reached 1.4×10^{-7} mol m⁻² s⁻¹ Pa⁻¹. In addition, the use of "LDH buffer layer" represented a new concept for facile in situ synthesis of well-intergrown ZIF-8 membranes. For instance, Liu further in situ prepared the vertically aligned ZnAl-CO₃ LDH buffer layers on γ -Al₂O₃ substrates (Fig. 6) [70]. The high length-to-width of LDH grains greatly facilitated nucleation and growth of ZIF-8 crystals. After in situ solvothermal growth, well-intergrown ZIF-8 membranes with the thickness ~20 μ m were prepared (Fig. 6(d)). Gas permeation results showed the SF of prepared ZIF-8 membrane reached 4.2, 10.0, and 12.5 for H₂/CO₂, H₂/N₂, and H₂/CH₄, respectively.

To enhance the gas selectivity of ZIF-8 membranes further, ZnAl-NO₃ LDH modified layers were calcined at 350 °C prior to solvothermal treatment with the ligand 2-methylimidazole. H₂/CH₄ gas selectivity of prepared ZIF-8 membranes reached ~83.1, which was by far the highest value ever reported for pure ZIF-8 membranes possibly due to the framework rigidization caused by neighboring ZnO nanocrystals [71]. To sum up, LDH complementary buffer layers not only enabled to guarantee the formation of well-intergrown ZIF membranes, but also facilitated their performance enhancement.

2.4. LDHs as transport channels for CO₂

Recently construction of facilitated transport membranes by establishing high-speed facilitated transport channels has been intensively investigated [72,73]. LDHs with specific interlayer spacing permit the rapid transport of smaller molecules (like CO₂). Wang proposed a calcination-reconstruction method to prepare MgAl-CO₃ LDH/PEIE (polyethyleneimine copolymerized with epichlorohydrin) facilitated transport membranes by designing high-speed CO₂ facilitated transport channels [74], which was schematically illustrated in Fig. 7. The active layer of prepared LDH/PEIE membrane was only 263 ± 15 nm. Prepared LDH/PEIE membrane displayed excellent CO₂ permselectivity by in situ reconstruction of calcined MgAl-CO₃ LDH fillers as high-speed facilitated transport channels. The CO₂ permeance reached 1.9×10^{-6} mol m⁻² s⁻¹ Pa⁻¹ with a CO₂/N₂ selectivity of 268 at the feed pressure of 0.11 MPa. To improve selectivity further, polyvinylamine (PVAm), a linear polymer containing abundant primary amine groups, was used as fixed-site-carrier membranes. The effect of divalent metal ions (Zn²⁺, Ni²⁺) in LDH nanofillers on the gas separation performance was further examined [75]. In addition, ZnAl-CO₃ LDH and NiAl-CO₃ LDH fillers also improved the CO₂/N₂ separation performance to a certain extent.

A summary of gas separation performance of LDH-based membranes was shown in Table 1. It was noted that LDH-based membranes with sub-nanometer sized gallery height exhibited accurate molecular sieving effect. In particular, in situ prepared ZIF-8@ZnAl-CO₃ LDH

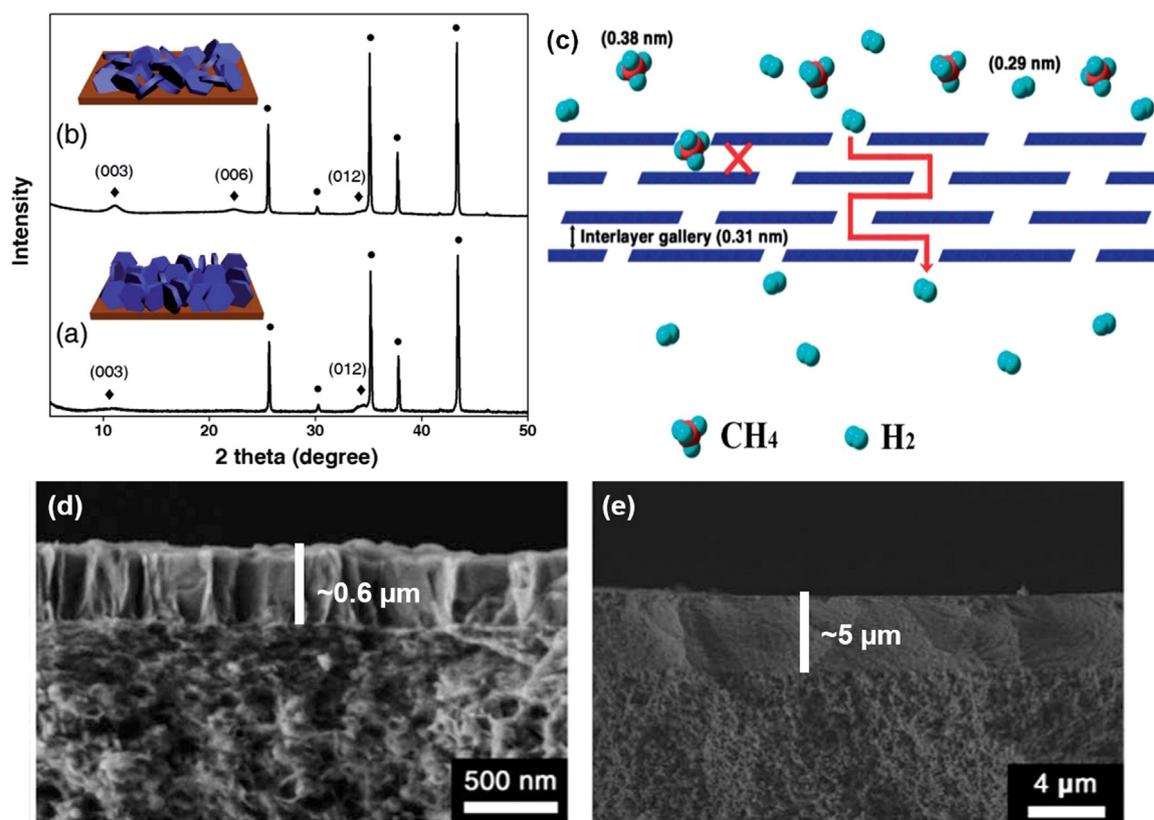


Fig. 4. XRD patterns of NiAl-CO₃ LDH membranes prepared with (a) DI-water and (b) CO₂-saturated water as solvents, respectively; (c) illustration of the concept of interlayer gallery-based separation and SEM images of NiAl-CO₃ LDH membranes prepared with (d) DI-water and (e) CO₂-saturated water as solvents, respectively. Reproduced with permission from Ref. [66]. Copyright © 2014, Royal Society of Chemistry.

composite membranes showed the gas selectivity significantly higher than single ZIF-8 or ZnAl-NO₃ LDH membranes. In addition, interlayer galleries of LDHs could serve as high-speed CO₂ facilitated transport channels within polymeric membranes for efficient CO₂ purification. It is therefore believed that LDHs may pave a brand-new avenue for designing and fabricating high-performance gas separation membranes.

3. LDH-based membranes for liquid separation

Recent decades witnessed significant progress made in membrane-based liquid separation technology, e.g. wastewater treatment [76,77], desalination [78,79], water recovery [80] and oil/water separation [81]. LDHs as a representative of clay materials had been employed in fabrication of LDHs/polymer nanocomposite membranes [82]. Several physicochemical properties of membranes (such as wettability [81], mechanical strength [62], thermostability [47], electroconductivity [83], flammability [39] and barrier properties [84]) have been proved to exert significant influence on the liquid separation performance of LDHs/polymer nanocomposite membranes.

3.1. LDHs as nanofiller for nanocomposite membranes

3.1.1. Ultrafiltration (UF) membranes

Versatile nanofillers have been added into the polymer matrix to improve the separation performance of UF membranes [85–87]. Among them, LDHs have been considered as a promising nanofiller for improving hydrophilicity, fouling resistance, mechanical strength, thermal stability and separation performance of UF membranes. Zhao [88] prepared ZnAl-LDH incorporated poly(ether sulfone) (PES) membranes with the phase inversion method and systematically investigated the effect of LDH doping content (0–3 wt%) on the separation

performance of PES membranes. LDH incorporated PES UF membranes achieved higher water permeability, superior protein removal efficiency as well as better antifouling properties. Oskoui [60] employed nano-layered MgAl-LDHs (Fig. 8(a)) as the hydrophilic nanofiller of polyvinylidene fluoride (PVDF) UF membranes. Results showed that nano-layered LDHs could significantly improve the separation performance of PVDF membranes in case N-methyl-2-pyrrolidone (NMP) was utilized as the solvent. Moreover, the pore shape varied from sponge-like to finger-like in the presence of LDHs nanofiller (Fig. 8). Nevertheless, water flux was decreased at high doping concentration (4.0 wt %) due to the unavoidable aggregation of LDH nanolayers. To minimize the aggregation, Zhang [56] proposed the use of exfoliated MgAl-LDHs as the nanofiller for preparation of positively charged hybrid PES UF membranes via phase inversion method. This membrane showed higher rejection rate (above 85%) for PEG 20000 and lower adsorption amount for positively charged proteins. Furthermore, novel charged mosaic PES membranes were prepared by incorporating positively charged MgAl-LDHs surface-grafted with sulfobetaine methacrylate [89]. It was found that charged mosaic PES UF membranes showed excellent dyes rejection rate (86.7% for Reactive Red 49), low salt rejection rate (9.3%, 7.6% and 0.53% for MgCl₂, Na₂SO₄ and NaCl, respectively) and high pure water flux (80.2 L m⁻² h⁻¹) under 0.4 MPa.

3.1.2. Nanofiltration (NF) membranes

NF membranes have been widely employed in wastewater treatment and desalination [90]. Zhang [56] utilized exfoliated MgAl-LDHs as inorganic additives for fabrication of PES NF membranes. Prepared NF membranes showed considerably high rejection rate for PEG400 but much lower rejection rate for MgSO₄. In response to this issue, exfoliated hydrotalcite/graphene oxide (EHT/GO) hybrid nanosheets were synthesized via flocculation deposition (schematically shown in

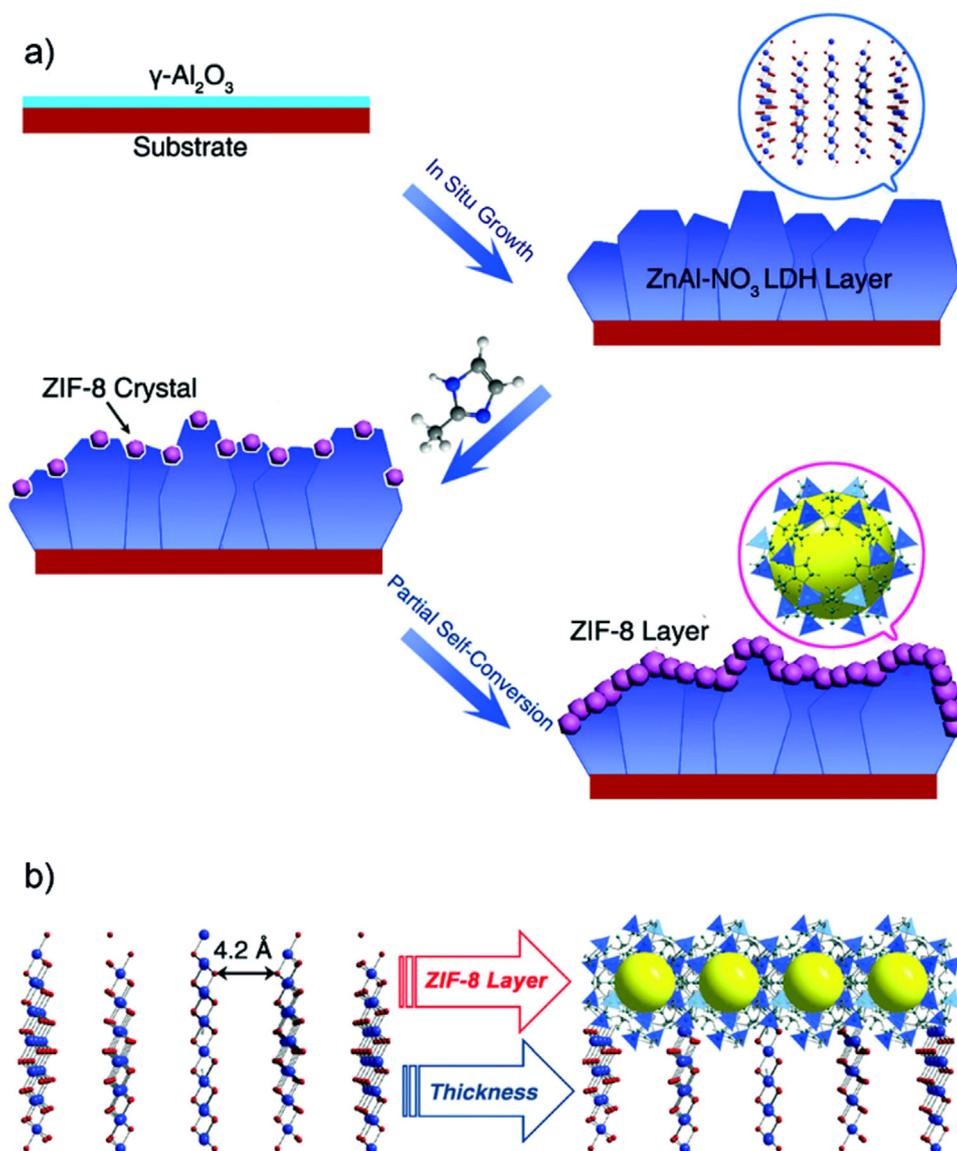


Fig. 5. a) Illustration of preparation of the ZIF-8@ZnAl-NO₃ composite membrane on a γ -Al₂O₃-modified α -Al₂O₃ substrate via partial self-conversion method of the ZnAl-NO₃ LDH precursor layer; b) structural change of the ZnAl-NO₃ LDH membrane after the solvothermal treatment with 2-methylimidazole. Reproduced with permission from Ref. [68]. Copyright © 2015, Wiley-VCH Verlag GmbH & Co. KGaA, Weinheim.

Fig. 9(a)) [57]. After being uniformly dispersed in polyethyleneimine (PEI) aqueous solution, compact NF thin-film nanocomposite (TFN) membranes (Fig. 9(e)) constructed by EHT/GO hybrid nanosheets were fabricated via interfacial polymerization (IP). Desalination experiment illustrated that incorporation of EHT/GO hybrid nanosheets into PA layer of TFN membranes effectively increased water flux to $26 \text{ L m}^{-2} \text{ h}^{-1}$ at 0.8 MPa. Simultaneously, the MgCl₂ rejection ratio of EHT/GO membranes maintained at 97.0%.

3.1.3. Forward osmosis (FO) membranes

Past decades witnessed increasing attention paid to FO process due to low hydraulic pressure during operation, high rejection to a wide range of contaminants and enhanced anti-fouling properties [91,92]. Nevertheless, fabrication of high performance FO membranes remained a great challenge facing their practical applications [62]. Recent studies indicated that LDHs could serve as excellent nanofiller for FO thin-film composite (TFC) membranes. For instance, LDH nanoparticles were uniformly blended in the polysulfone (PSf) substrate of TFN membrane to increase the porosity, hydrophilicity, mechanical strength and thermal stability, which in turn were favorable for reducing internal

concentration polarization (ICP) and enhancing water permeability [62]. After doping with 2 wt% LDHs, a $\sim 42.5\%$ increase in water flux of TFN membranes was achieved without compromise in reverse salt flux. Furthermore, Wang [93] prepared LDH modified-graphene oxide (LDH/GO) hybrid nanoparticles as the nanofiller of PSf substrates. Owing to omission of an additional drying step, dispersion condition of GO nanosheets was remarkably improved, resulting in significant improvement of salt rejection.

Cussler [94] proposed that layered materials could serve as effective additive for enhancing anti-corrosion and anti-fouling properties of original FO membranes. For instance, to further enhance chlorine and fouling resistance, LDH nanoparticles were directly bound on the surface of TFC membranes via polydopamine-induced immobilization process [84]. Excellent chlorine-resistant performance (~ 96 times high than bare TFC membranes) was then confirmed by the accelerated chlorination experiment (Fig. 10(c)). Simultaneously, LDH-modified TFN membranes exhibited superior anti-fouling capability (Fig. 10(b)). In addition, Pardeshi [61] investigated the influence of LDH content on the separation performance polyvinyl chloride (PVC) TFN membranes. It was observed that increasing LDH contents within PVC substrate

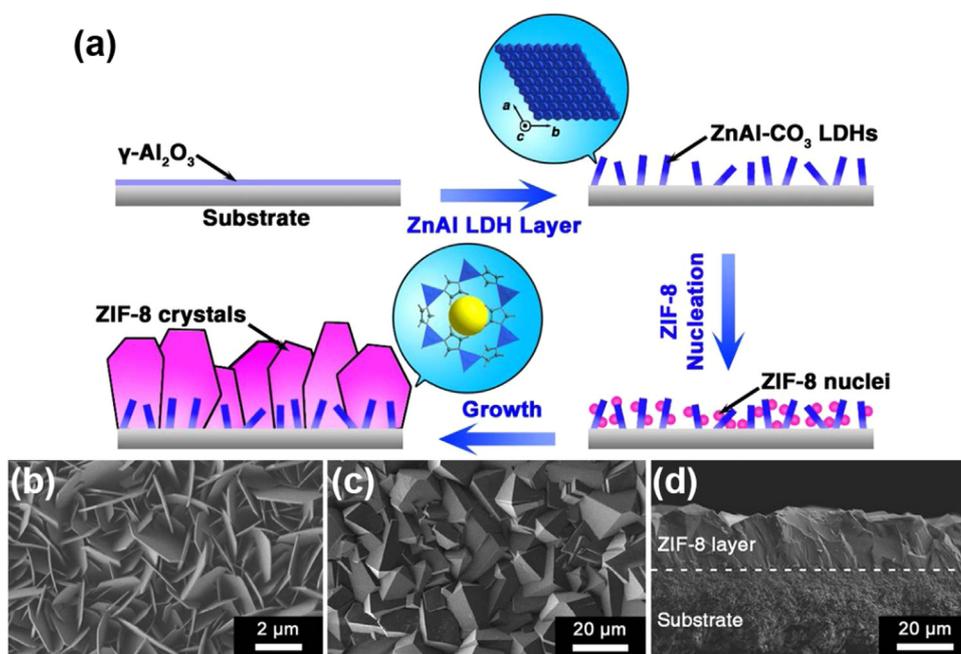


Fig. 6. (a) Illustration of ZIF-8 membrane growth on the ZnAl-LDH buffer layer-modified γ - Al_2O_3 substrate by in situ solvothermal growth; (b) the SEM image of the ZnAl- CO_3 LDH buffer layer, and SEM images of the (c) top and (d) cross-section of prepared ZIF-8 membrane. Reproduced with permission from Ref. [70]. Copyright © 2014, American Chemical Society.

induced an increase in water flux of TFN membranes. To sum up, above-mentioned studies demonstrated that incorporation of LDHs as nanofillers played an important role for performance improvement of TFN membranes.

3.2. LDHs as adsorbents for membrane adsorption

Early attempts evidenced that LDHs excellent adsorbents for removal of harmful diverse cations and anions (such as Pb^{2+} , Cd^{2+} , Cu^{2+} , arsenate, chromate and phosphate) from aqueous solutions relying on both surface adsorption and anion exchange of charge compensating anions located in interlayer galleries [95–101]. In addition, the unique “memory effect” of calcined LDHs, also known as layered double oxides (LDOs) [102], could be also utilized as cost-effective and energy-efficient adsorbents [48]. Membrane adsorption represents an emerging adsorption technology for wastewater treatment [103]. LDHs

have attracted considerable attention for potential applications in membrane adsorption processes. Duan [104] prepared LDH/eggshell membranes (ESM) for Cr(VI) removal with an in situ hydrothermal crystallization method. Results indicated that prepared MgAl-Cl LDH/ESM composite membranes (Fig. 11) could be efficient adsorbents for Cr(VI) (adsorption capacity was 27.9 mg/g) removal even under the condition that pH values were adjusted by addition of acid. A removal efficiency higher than 90% was obtained after an elapse of only 30 min (Fig. 11(f)). Visvanathan [105] was devoted to developing high performance adsorption-based hybrid membranes for continuous removal of high concentration perfluorooctanoic acid (PFOA), one of the major perfluorinated compounds contaminating global water sources. A removal efficiency as high as 95% could be achieved by incorporating MgAl-LDHs into NF membranes without any adverse effect on flux as compared with direct membrane filtration. A 30% increase in rejection rate for LDH-based hybrid NF membranes was attributed to the

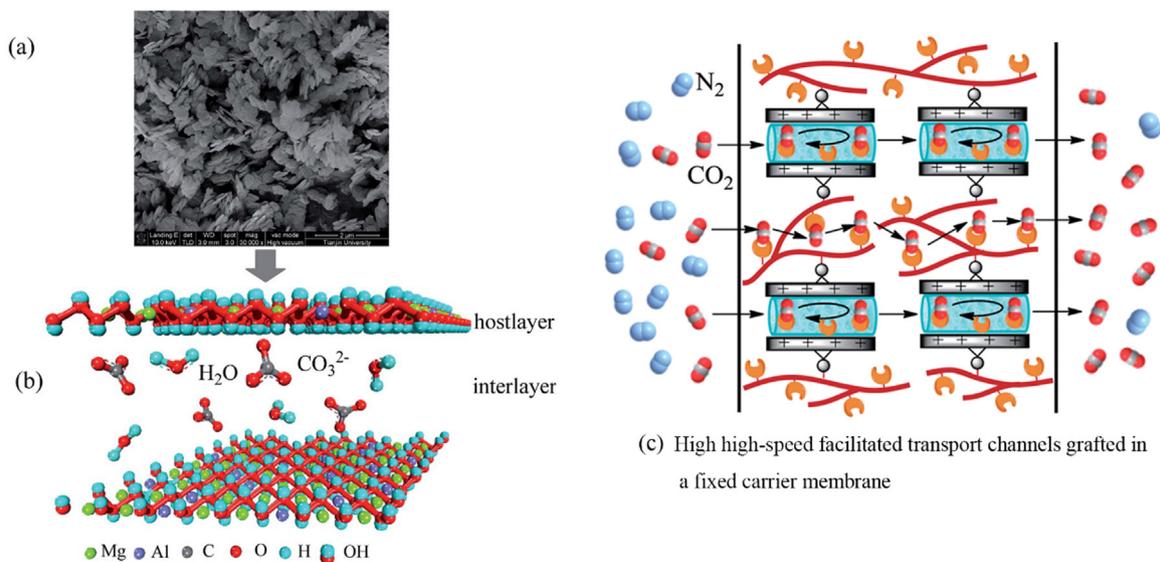


Fig. 7. Structural demonstration of LDHs and LDH-modified polymer membranes: (a) SEM image of carbonate-intercalated LDHs with about 110 nm size; (b) schematic drawing of carbonate-intercalated LDHs; and (c) carbonate-intercalated LDHs grafted fixed carrier membrane with the high-speed facilitated transport channels. Reproduced with permission from Ref. [74]. Copyright © 2014, Royal Society of Chemistry.

Table 1
Gas separation performance of LDH-based membranes.

Membranes	Function of LDHs	Performance of gas separation	References
MgAl-CO ₃ LDH on α -Al ₂ O ₃ substrate	As separating layers	SF _{CO₂/N₂} = 35 P _{CO₂} = 2.07×10^{-7} mol m ⁻² s ⁻¹ Pa ⁻¹ (Single-gas, 25 °C, 0.21 MPa)	[64,65]
NiAl-CO ₃ LDH on α -Al ₂ O ₃ substrate	As separating layers	SF _{H₂/CH₄} = 78.7 P _{H₂} = 4.6×10^{-8} mol m ⁻² s ⁻¹ Pa ⁻¹ (1:1 mixture (H ₂ -CH ₄), 180 °C, 0.1 MPa) P _{H₂} = 5.2×10^{-8} mol m ⁻² s ⁻¹ Pa ⁻¹ (1:1 mixture (H ₂ -CH ₄), 210 °C, 0.1 MPa)	[66,67]
ZnAl-CO ₃ LDH on α -Al ₂ O ₃ substrate	As separating layers	SF _{H₂/CH₄} = 13.7 P _{H₂} = 3.7×10^{-8} mol m ⁻² s ⁻¹ Pa ⁻¹ (1:1 mixture (H ₂ -CH ₄), 180 °C, 0.1 MPa)	[67]
ZIF-8@MgAl-CO ₃ LDH composite	As supporting layers	SF _{H₂/CH₄} = 12.9 P _{H₂} = 1.4×10^{-7} mol m ⁻² s ⁻¹ Pa ⁻¹ (1:1 mixture (H ₂ -CH ₄), 25 °C, 0.1 MPa)	[69]
ZIF-8@ZnAl-NO ₃ LDH composite	As supporting layers	SF _{H₂/CH₄} = 12.5 P _{H₂} = 1.4×10^{-7} mol m ⁻² s ⁻¹ Pa ⁻¹ (1:1 mixture (H ₂ -CH ₄), 25 °C, 0.1 MPa)	[70]
ZIF-8@ZnAl-NO ₃ LDH composite	As supporting precursor layers	SF _{H₂/CH₄} = 83.1 P _{H₂} = 1.9×10^{-8} mol m ⁻² s ⁻¹ Pa ⁻¹ (1:1 mixture (H ₂ -CH ₄), 30 °C, 0.1 MPa)	[71]
MgAl-CO ₃ LDH/PEIE composite	As transport channels	SF _{CO₂/N₂} = 268 P _{CO₂} = 1.9×10^{-6} mol m ⁻² s ⁻¹ Pa ⁻¹ (15:85 mixture (CO ₂ -N ₂), 25 °C, 0.11 MPa)	[74]
MgAl-CO ₃ LDH/PVAm composite	As transport channels	SF _{CO₂/N₂} = 296 P _{CO₂} = 1.1×10^{-6} mol m ⁻² s ⁻¹ Pa ⁻¹ (15:85 mixture (CO ₂ -N ₂), 25 °C, 0.11 MPa)	[75]

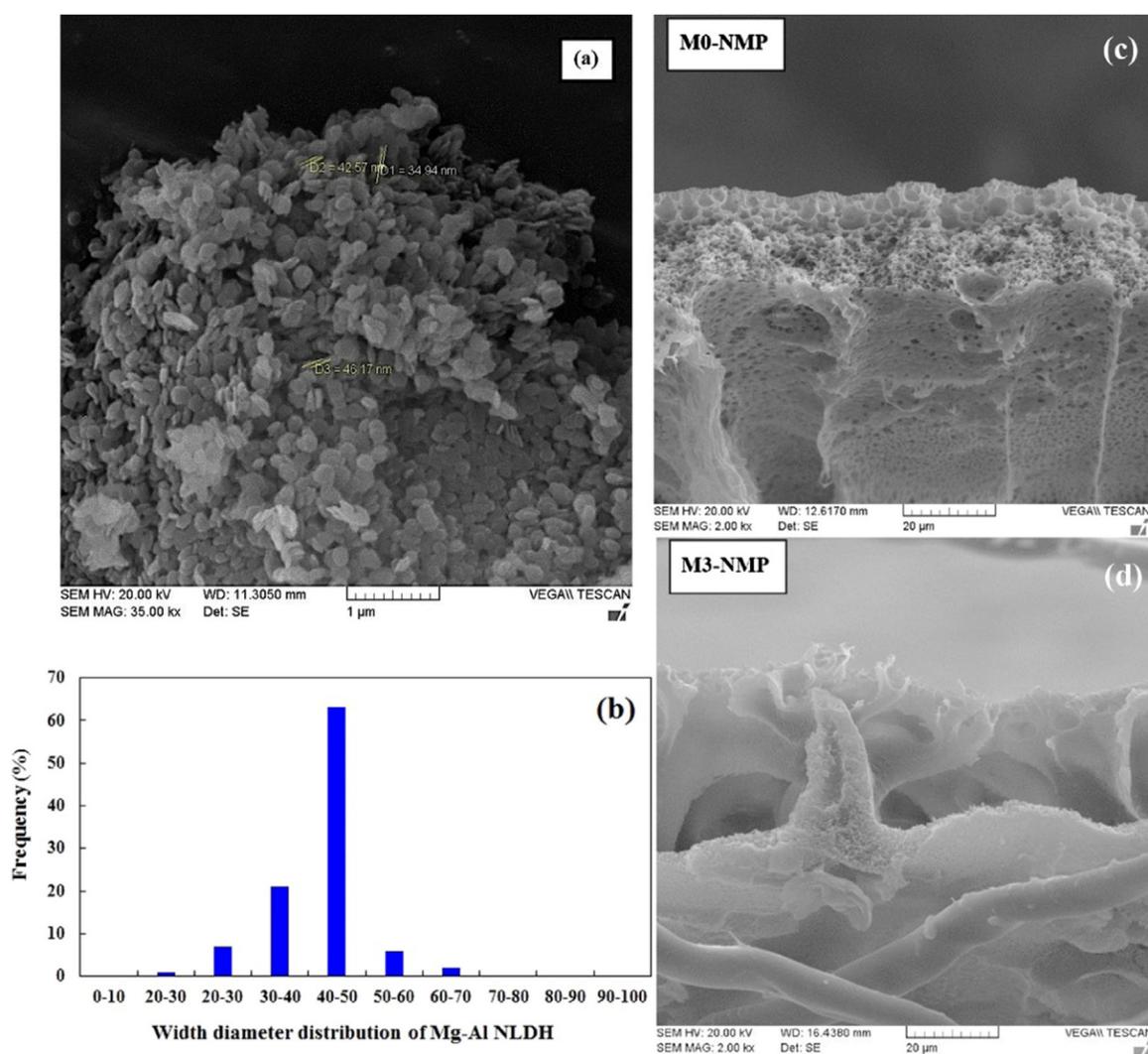


Fig. 8. (a) SEM image of nano-layered MgAl-LDHs; (b) width diameter distribution of the LDHs, and cross-sectional SEM images of (c) pure PVDF membranes and (d) LDHs/PVDF nanocomposite membranes (LDHs loading: 3 wt%). Reproduced with permission from Ref. [60]. Copyright © 2017, Elsevier.

formation of dense MgAl-LDH layers on membrane surfaces. Recently, Jia [58] incorporated exfoliated Mg-Al-Fe LDH nanosheets in PES membranes for efficient removal of phosphate and fluoride. Prepared composite membranes displayed higher adsorption capacity for

phosphate (5.61 mg/g) and fluorides (1.61 mg/g) than un-exfoliated materials.

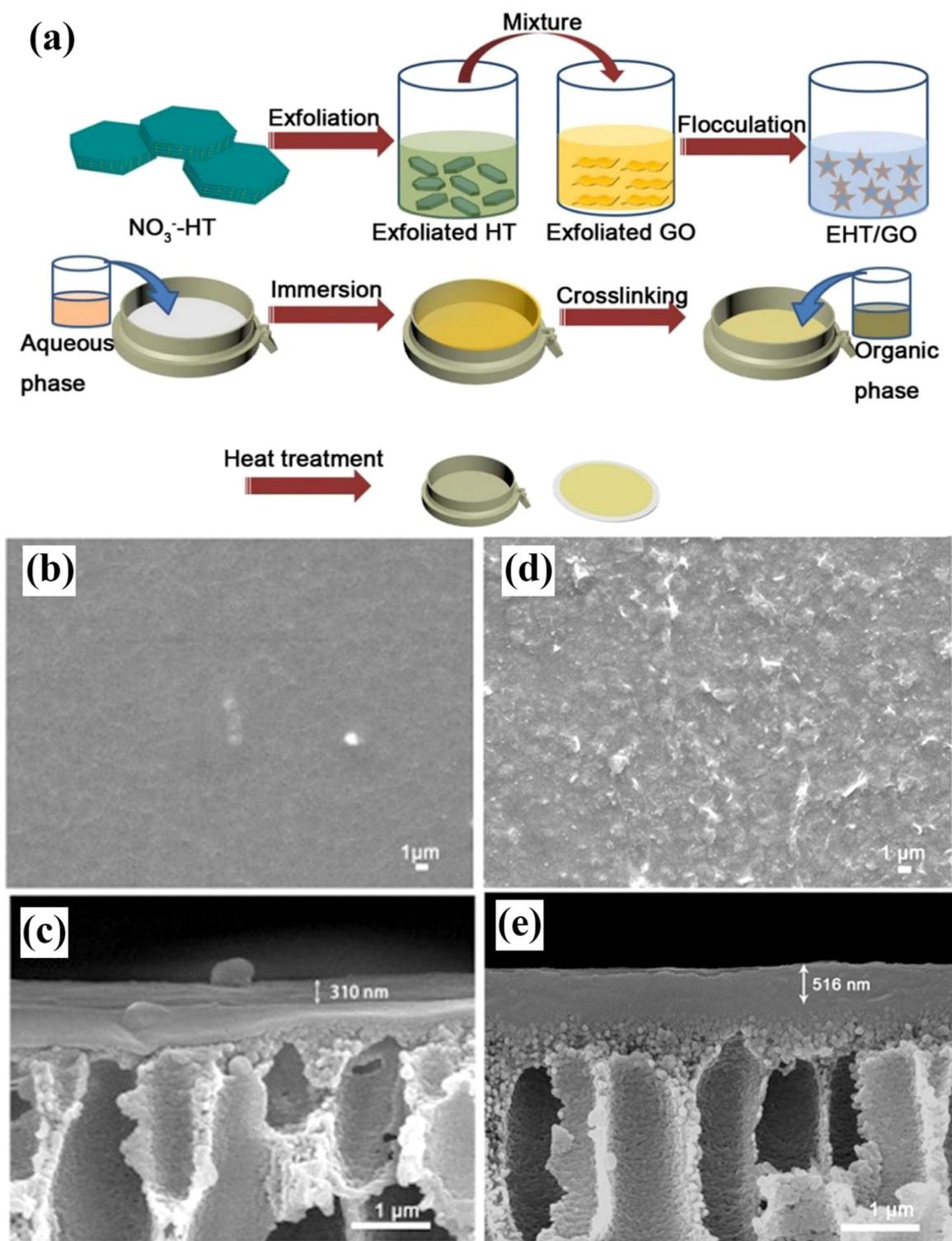


Fig. 9. (a) Illustration of the synthesis of EHT/GO hybrid nanosheets and the preparation of EHT/GO TFN nanofiltration membranes; SEM images of the top layer of TFN membranes with (b) 0 wt% and (d) 0.24 wt% EHT/GO loadings; and SEM images of the cross-section of TFN membranes with (c) 0 wt% and (d) 0.24 wt% EHT/GO loadings. Reproduced with permission from Ref. [57]. Copyright © 2017, Elsevier.

3.3. LDHs as hydrophobic layer for oil/water separation

Efficient oil/water separation represents the major environmental challenge due to the ever-increasing oil-containing wastewater discharge as well as increasingly frequent accidents of oil spill [106,107]. Membrane technology represents an effective approach for efficient oil/water separation [108]. Several studies have been carried out for

developing LDH nanosheet-based oil/water separation membranes. For instance, Liu reported the fabrication of commercial textiles functionalized with LDH microcrystals as well as low-surface-energy molecules (schematically shown in Fig. 12(I)) [109]. Results showed that prepared textiles could be employed as not only high-performance oil/water separation membranes (separation efficiency > 97%), but also “bags” for selective oil recovery from aqueous suspension (Fig. 12(a)-(h)).

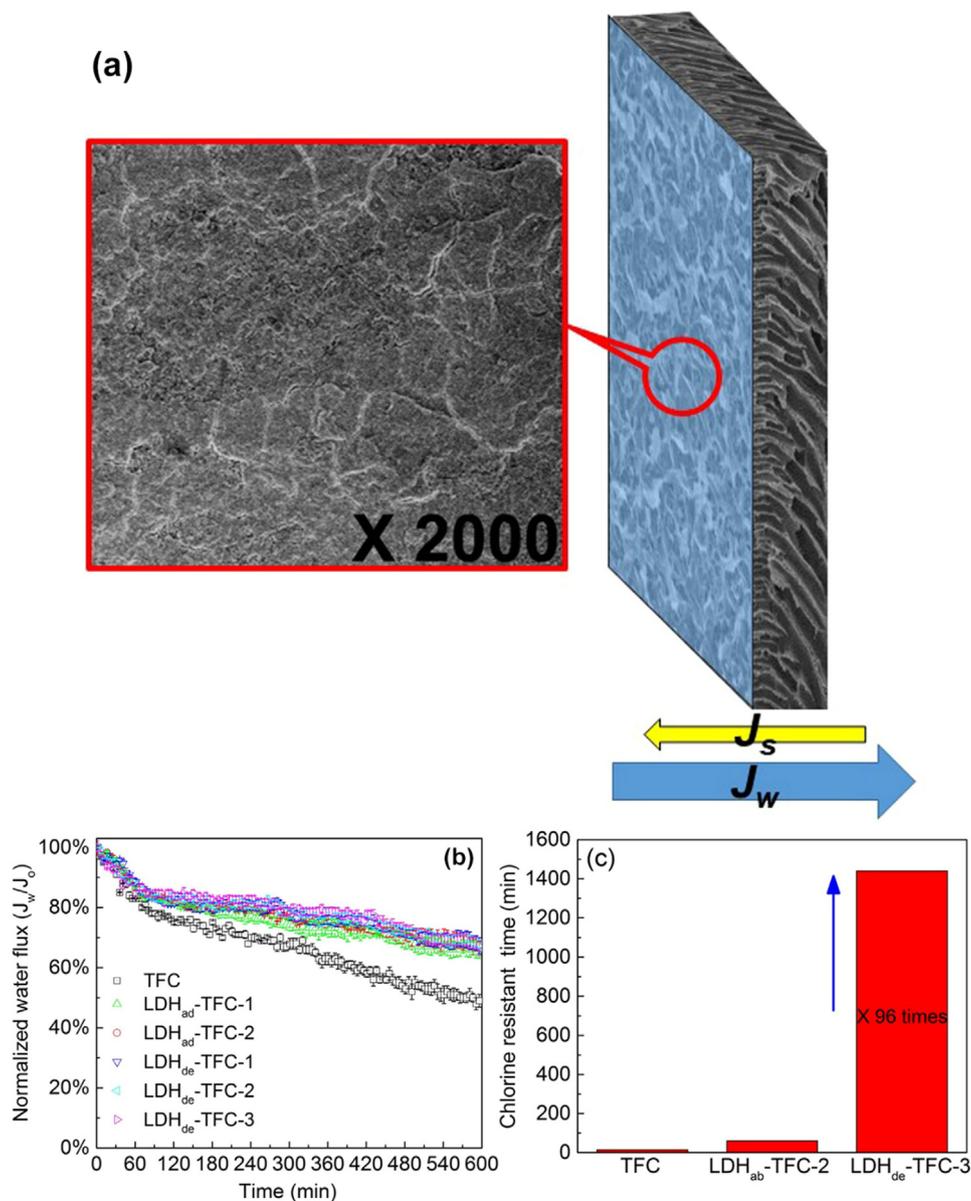


Fig. 10. (a) The schematic diagram of the LDHs deposition modified TFC membranes; (b) the normalized water fluxes of the unmodified and modified membranes at alginate fouling tested in FO mode; and (c) the chlorine resistant time of TFC, LDH_{ab} -TFC-2 and LDH_{de} -TFC-3 membranes by immersion in 1000 ppm NaOCl solution. Reproduced with permission from Ref. [84]. Copyright © 2017, Elsevier.

With an electrospun-nanofiber-templated in situ hydrothermal method, Shami [110] successfully introduced vertically aligned MgAl-LDH arrays on nanofibrous poly(acrylonitrile) (PAN) membranes which subsequently were surface-modified with cyclohexanecarboxylic acid. Prepared superhydrophobic/superoleophilic nanofabrics not only were capable of repelling both drinkable hot water ($\sim 95^\circ\text{C}$) and cool water ($\sim 25^\circ\text{C}$) but also allowed preferential permeation of oils across the membrane. An excellent oil recovery efficiency (including chloroform, toluene, *n*-heptane, hexadecane and motor oil) was then demonstrated.

Wu [81] employed a facile layer-by-layer self-assembly method for constructing 3D hierarchical membranes on porous cellulose acetate substrates surface-modified with sepiolite-grafted LDHs. Prepared membranes exhibited high flux and excellent underwater superoleophobic behaviors relying on the hierarchical microstructure. Recently, a simple and effective method was developed to prepare superhydrophobic cellulose/LDH membranes in an open oil/water two-phase system [111]. Prepared membranes exhibited high separation efficiency ($> 95.0\%$), excellent recyclability and stable

superhydrophobicity under harsh conditions, making them superb candidate for remediation of oily waste water. To sum up, above-mentioned studies demonstrated that microstructure optimization of LDH modified layers played a critical role in enhancing the oil/water separation performance.

3.4. LDHs as ionic conductors for direct methanol fuel cells (DMFC)

In comparison with traditional batteries, direct methanol fuel cell (DMFC) has become the focus of people's interest. Nevertheless, unavoidable crossover of methanol fuel, which seriously degrades the cell performance, remains a major hindrance to DMFC's industrialization [83,112]. Recently great efforts have been made to develop new types of anion exchange membranes for solving the methanol crossover problem. As a representative of anionic clays, LDHs remained stable in an alkaline media. For instance, Lee proposed fabrication of LDH-modified Nafion membranes by incorporating LDH nanosheets with different Mg^{2+}/Al^{3+} ratios for DMFC [113]. Nano-sized LDH-modified

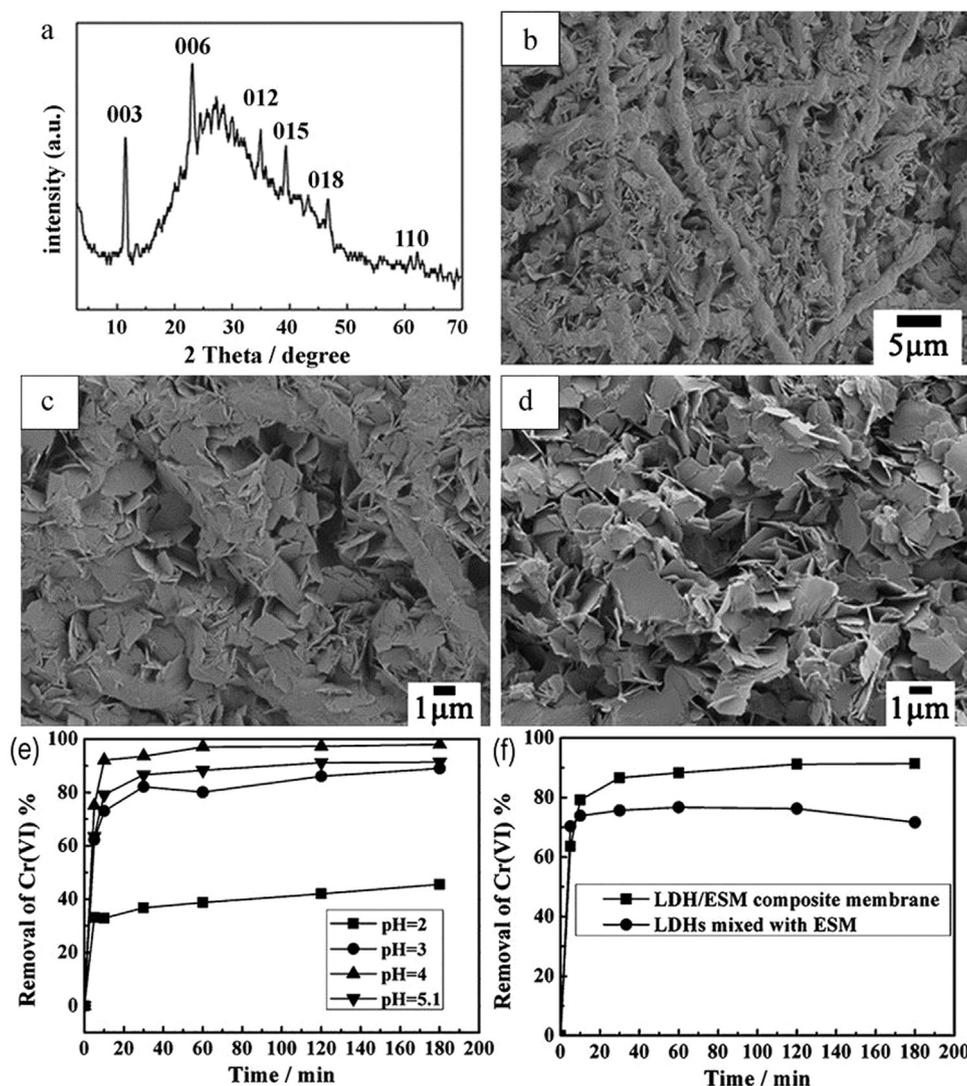


Fig. 11. (a) XRD pattern of the MgAl-Cl LDH/ESM composite membrane; SEM images of MgAl-Cl LDH/ESM composite membranes (b, c) top and (d) cross-section; (e) demonstration of the effect of pH values on Cr(VI) removal efficiency and (f) demonstration of the kinetics of Cr(VI) removal efficiency. Reproduced with permission from Ref. [104]. Copyright © 2014, American Chemical Society.

polyelectrolyte membranes reached a better balance between diffusion coefficient and ionic conductivity at high methanol feed concentrations (7 M). Nicotera [114] employed LDHs as nano-additives of Nafion-based membranes for H_2 /air-fed fuel cells. Influences of Mg^{2+}/Al^{3+} metal ratio (2:1 and 3:1) and the type of interlayer anions (CO_3^{2-} , ClO_4^- , NO_3^-) on proton conductivity of LDH/Nafion nanocomposite membranes were systematic investigated. Tsotsis [115] prepared high performance LDH/poly(ether ether ketone) (SPEEK) nanocomposite membranes by in situ sulfonation of SPEEK and LDH films for DMFC. Prepared LDH/SPEEK nanocomposite membranes showed not only considerably high proton conductivity and low methanol diffusivity but also excellent performance comparable with commercial Nafion membranes. Lee [116] incorporated MgAl and NiTi LDHs into SPEEK membranes, respectively. Proton conductivity measurement indicated that MgAl-LDH/SPEEK nanocomposite membranes showed higher proton conductivities than that of NiTi-LDH/SPEEK membranes.

Zhao [117] synthesized crosslinked poly (vinyl alcohol)/MgAl- CO_3 (PVA/LDH) hybrid anion-exchange membranes for DMFC. It was found that incorporating 20 wt% LDHs into PVA matrix resulted in not only higher ionic conductivity but also lower ethanol permeability. The performance test of the DMFC using the PVA/LDH hybrid membrane demonstrated that the fuel cell yielded a power density of 82 mW cm^{-2}

at 80°C , which was much higher than that of the DMFC employing quaternary ammonium group functionalized PVA membranes. Similarly, Herrero [83] prepared sulfonated polysulfone (SPSU)/LDH composite proton exchange membranes for DMFC. Introduction of LDHs significantly affected water uptake amounts, electrical properties and transport behaviors of SPSU membranes. Impedance plots as a function of LDH addition amounts were then measured and shown in Fig. 13(a). It was observed that the diameter of the high frequency arcs decreased with the addition amount of LDHs, therefore indicating an enhanced proton conductivity by increasing LDH addition amounts. In addition, SPSU/LDH nanocomposite membranes exhibited superior electrical performance compared with pure SPSU membranes (Fig. 13(b)). Sun [118] fabricated novel charge-guided ion transport hybrid membranes consisting of anionic GO and cationic CoAl (or MgAl) LDH nanosheet superlattice units. Relative selectivity of prepared hybrid membranes towards monovalent and trivalent cations reached as high as 30 therefore indicating a synergistic effect originating from the molecular-scale cooperative hetero-assembly of GO and LDH nanosheets which played a dominant role in charge-guided ion filtration and separation.

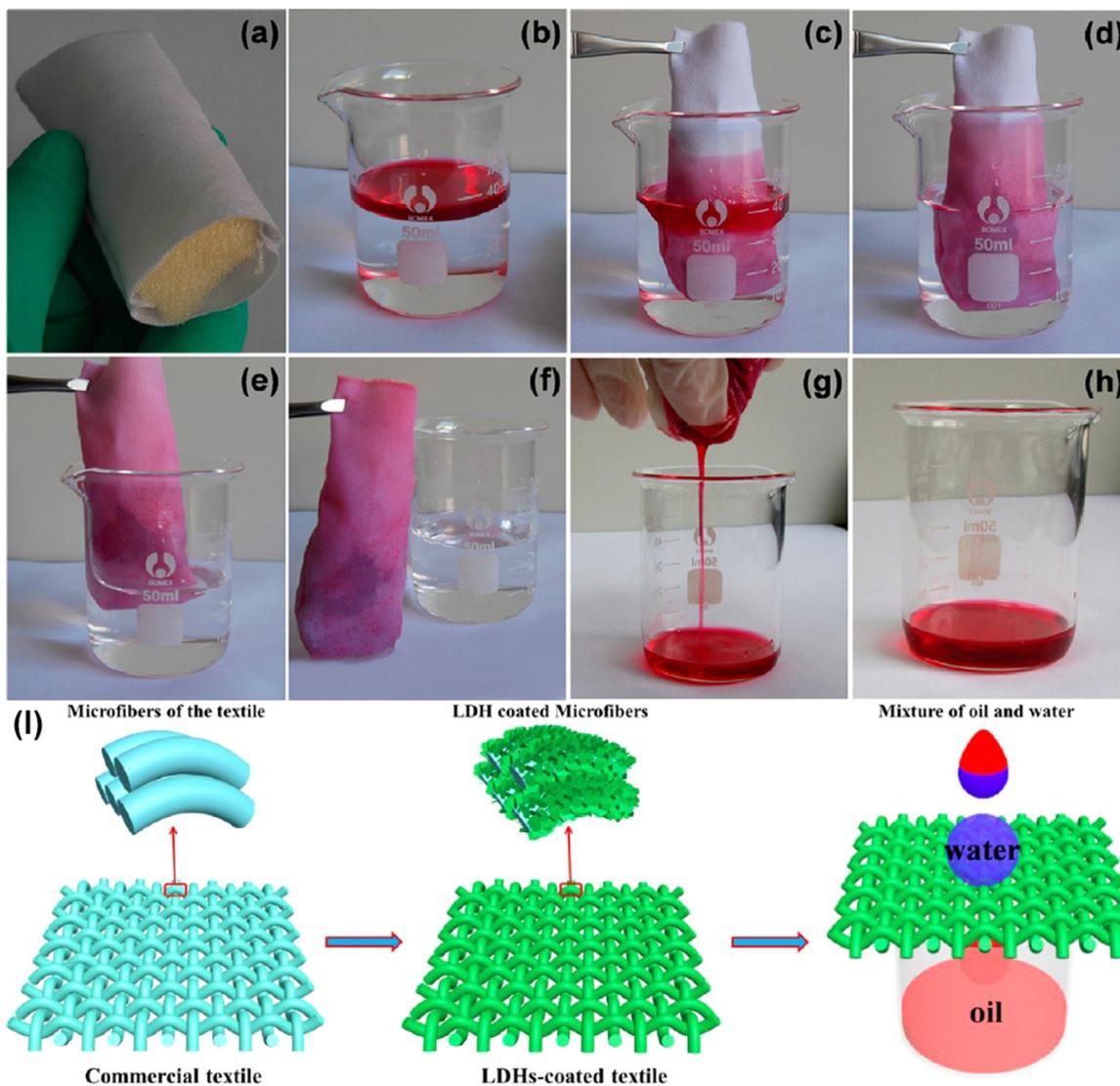


Fig. 12. Digital photographs of (a) the textile bag and (b – g) the oil adsorption and recycling process with the superhydrophobic textile bag; (i) schematic diagram of the modification of commercial textile with LDH and its application for oil/water separation. Reproduced with permission from Ref. [109]. Copyright © 2015, American Chemical Society.

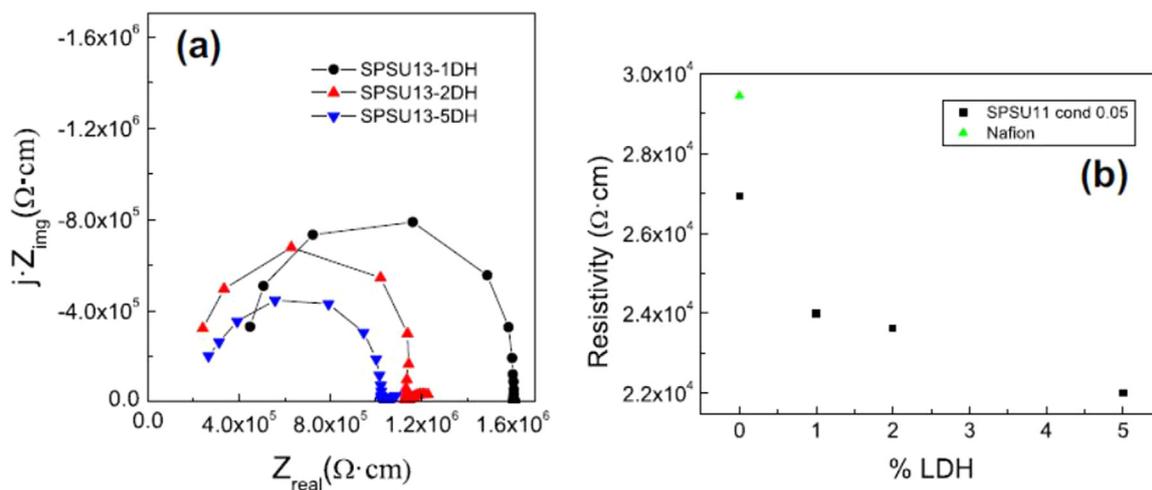


Fig. 13. (a) Nyquist plot of three composite membranes with different LDH (1%, 2% and 5%) loadings ($c = 0.05 \text{ M HCl}$); (b) Resistivity of commercial Nafion membranes with different LDH loadings. Reproduced with permission from Ref. [83]. Copyright © 2013, Hydrogen Energy Publications, LLC. Publish by Elsevier.

4. Opportunities and challenges facing LDH-based separation membranes

LDHs as a representative of 2D materials have injected new vitality into membrane-based separation process. Compared with other 2D membrane materials, LDHs are unique in terms of 1) simple preparation process and low manufacturing cost; 2) uniform and tailorable gallery height; 3) rich surface functionality; 4) unique memory effect and regenerability; 5) excellent exfoliation capability; 6) excellent anti-fouling capacity; 7) easy scale-up and 8) considerable stability. These features have provided an avenue to design high-performance separation membranes. For instance, 1) compared with the relatively complicated manufacturing process of other 2D (like GO, 2D MOF, 2D COF, 2D zeolite, TMDC, MXene and $g\text{-C}_3\text{N}_4$) molecular sieve membranes, defect-free LDH membranes could be prepared in one step [66,67]; 2) relying on the uniform and tailorable interlayer gallery, LDH membranes have exhibited pronounced molecular sieving property for gas separation; in contrast, it remained a challenging task to maintain a uniform gallery height for most other 2D separation membrane, although some progress has been made in recent days [119,120]; 3) specific memory effect of LDHs has made it possible to construct high-speed facilitated transport channels for effective CO_2 purification [74,75] and effective removal of harmful diverse cations/anions [104,105]; 4) LDHs could be further exfoliated and serve as nanofillers for preparation of MMMs showing lower adsorption amount for positively charged pollutants, relying on unique electrostatic repulsive forces [56]. Combine with the functional diversity, commercial availability, low cost, stability and anti-fouling capacity, LDH-based membranes have shown excellent separation performance in diverse fields.

Nevertheless, a major challenge facing high performance LDH-based membrane fabrication resides in an accurate control of the interlayer spacing for specific separation. Furthermore, since the separation performance of LDHs-based membranes strongly depends on their microstructures (like the preferred orientation, grain boundary defects and thickness), facile methods for deliberate control of their microstructures are yet to be developed.

5. Conclusion

Relying on the uniform interlayer gallery, pure LDHs membranes have exhibited pronounced molecular sieving property for gas separation. Moreover, carbonate-intercalated LDHs could be further employed as competent high-speed facilitated transport channels for efficient CO_2 separation. In addition, LDHs could serve as competent buffer layers guaranteeing the formation of high performance MOF membranes. Further incorporation of LDHs into polymeric matrices resulted in the formation of nanocomposite membranes with significantly improved wettability, mechanical strength, thermostability, electroconductivity, chlorine-resistant and anti-fouling capability for efficient liquid separation. Taking consideration of the fact that LDHs can be further exfoliated into monodispersed nanosheets or chemically modified for improving the affinity interaction with the polymer matrix, it is anticipated that employment of LDHs may provide an avenue to design the next generation of high-performance separation membranes.

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